

WA2: Hybrid Ceramic Membrane Filtration in Water Treatment Pilot tests at WWTP Almelo

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WP22 Hybrid ceramic membrane systems (KWR, FHNW)

- HCMS offer improved rejection of dissolved compounds and optimal control of fouling of membrane fouling (Lab-scale study in TECHNEAU.
- WP22 aims at investigate the potential of HCMS at pilot scale and to optimize the overall performance for the removal of emerging contaminants.





Hybrid Ceramic Membrane Filtration

- Coagulation-CMF
- PAC-CMF

IX-CMF

• 03-CMF

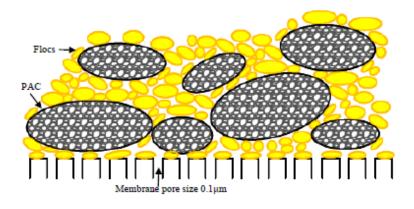


Figure 34: Possible formation and structure of PAC cake layer fouling on continuous with backwash channel

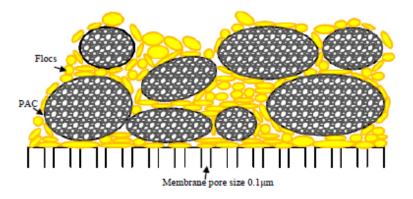


Figure 35: Possible formation and structure of PAC cake layer fouling on continuous without backwash channel



Pilot locations

- WWTP Almelo (The Netherlands)
- WWTP Basel (Switzerland)





WWTP Almelo

Design capacity: 5200 m³/h



- Process:
 - mechanical pre-treatment (screening, grit removal)
 - activated sludge treatment operated (sequencing-batch-reactor)
 - nutrient removal by nitrification-denitrification and simultaneous phosphorous removal by precipitation

| WWTP Almelo effluent quality (2014) | | | | |
|-------------------------------------|------|----------|----|--|
| Parameter | Mean | St. dev. | n | |
| N total (mg/L) | 6,19 | 4,61 | 57 | |
| P total (mg/L) | 1,73 | 1,19 | 57 | |
| COD (mg/L) | 33,7 | 8,45 | 50 | |
| BOD(mg/L) | 2,32 | 1,50 | 50 | |



Demonstration of promising technologies to address emerging pollutants in water and waste water

PAC-CMF pilot at WWTP Almelo

Membrane area : 2x 0,4 m²

Nominal pore size : 0,1 µm

Operation : dead-end













- Experiments: (1) OMP removal (2) Operational stability
- WWTP effluent + OMPs = Feed pilot plant.
- Cocktail of OMPs dosed, each ≈1μg/L.
- PAC dose (mg/L): 0, 15, 30, 60 [precoat mode]
- BW: pressurized (5 bar) with permeate and air
- CEB: BW with permeate and NaOCl

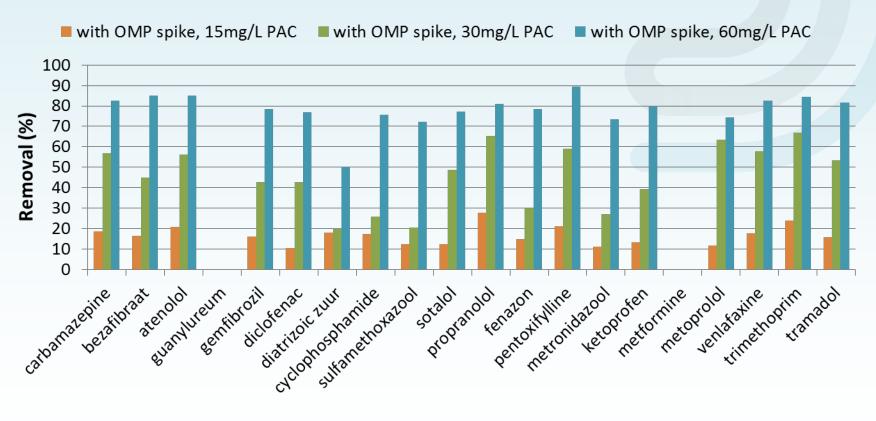
| Filtration time | 15 min |
|-----------------|--------------------------------------|
| Filtration flux | 60,80,100, 120 L/(m ² ·h) |
| BW frequency | 4 times per hour |
| BW time | <5 sec |
| CEB frequency | 1 time per 6 hour |
| Chemicals used | NaOCI (12,5 wt%) |
| Soaking time | 5 min |

| μg/L |
|-------|
| 0,936 |
| 0,953 |
| 0,901 |
| 0,951 |
| 0,962 |
| 0,881 |
| 1,027 |
| 0,972 |
| 0,849 |
| 0,973 |
| 0,980 |
| 0,999 |
| 0,918 |
| 1,019 |
| 1,005 |
| 0,996 |
| 0,797 |
| 0,970 |
| |



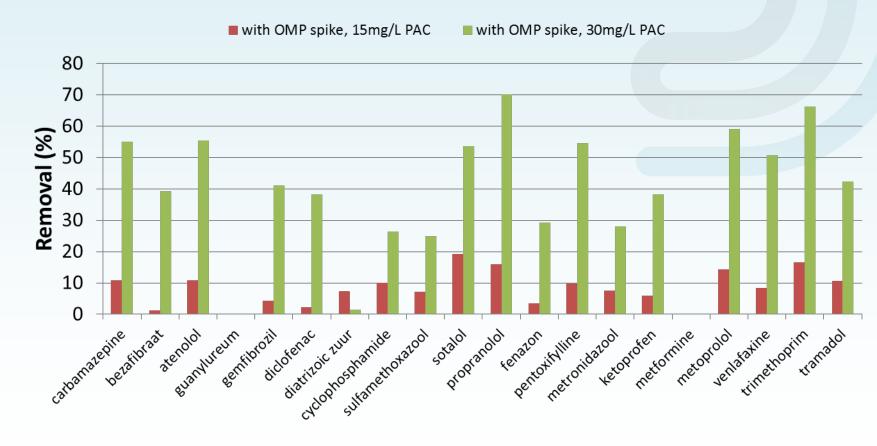
Removal of OMPs





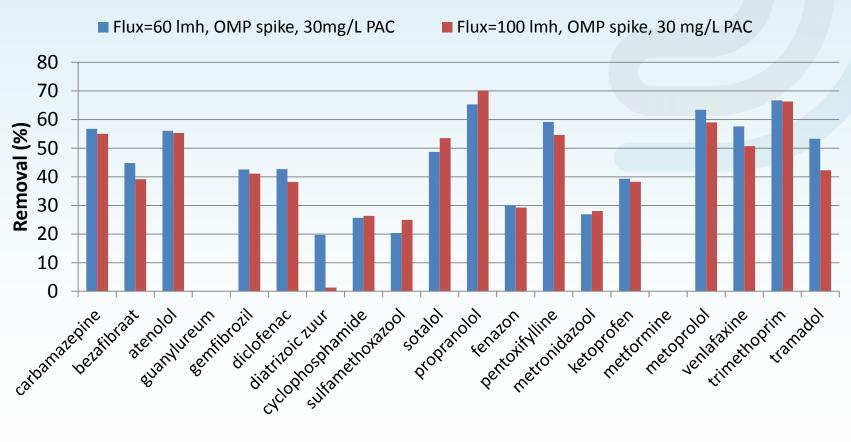








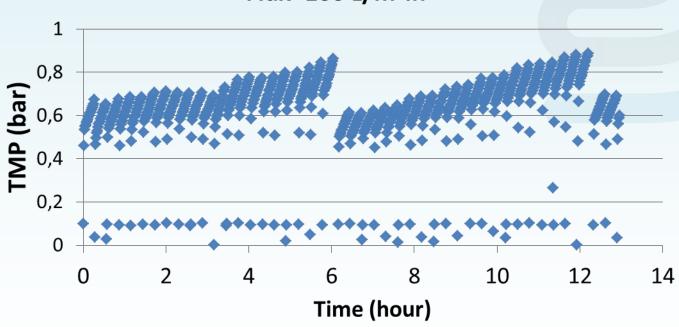
Effect of flux on OMP removal at 30 mg/L PAC dose





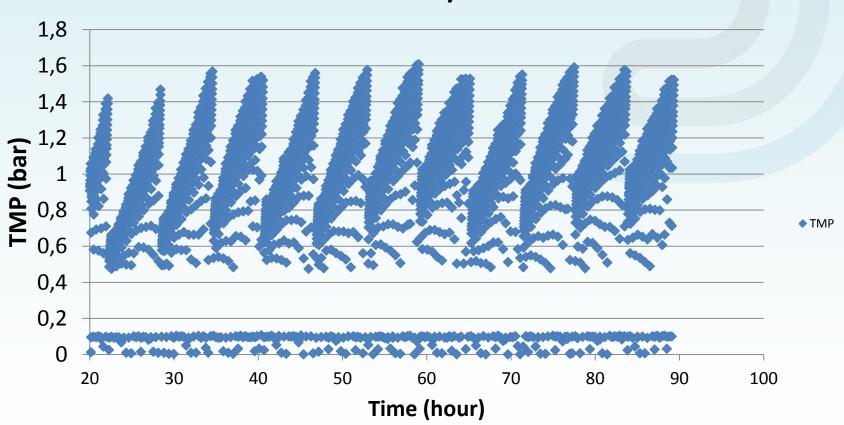
Process stability











Demonstration of promising technologies to address emerging pollutants in water and waste water

Conclusions

- Removal increases with PAC dose, as expected.
 However, it is not proportional to PAC dose.
- Precoating PAC on membrane surface increased average TMP.
- At 30mg/L PAC, the OMP removal was similar at flux=60 lmh and 100 lmh.
- CEB with NaOCl effectively recover the TMP.
- At 30mg/L PAC dose and flux=100 lmh, HCMF process remained stable for more than 5 days.



Demonstration of promising technologies to address emerging pollutants in water and waste water



Thanks for attention!